



# Solutions for CO<sub>2</sub> transport

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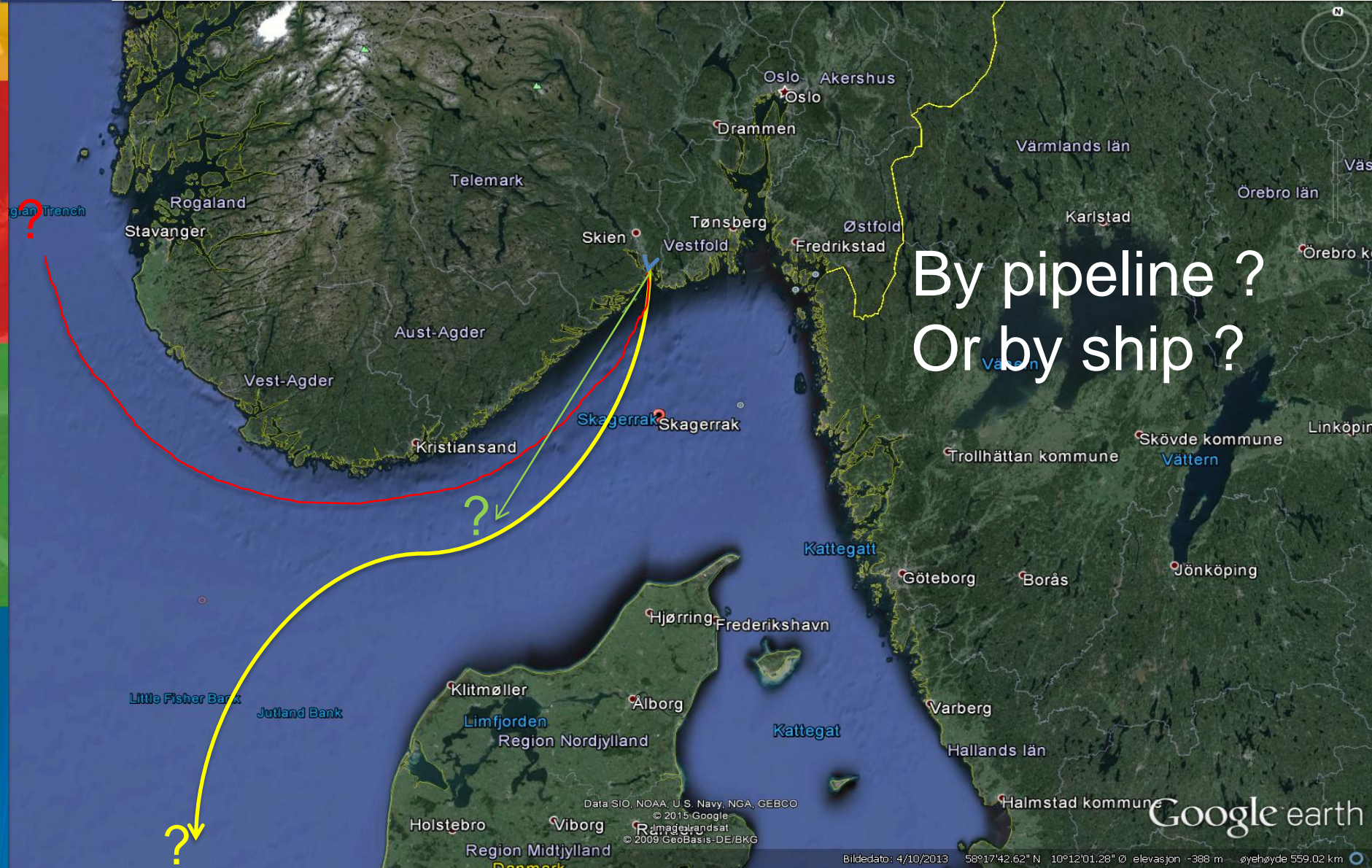
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Norcem CO<sub>2</sub> Capture Project

International CCS Conference May 20 – 21st 2015



# Taking CO<sub>2</sub> from Brevik to where?



By pipeline ?  
Or by ship ?



# The transport chain

1. Preparation for transport
  - Compression and drying
  
2. Transport
  - Pipelines
  - Ships, compressed CO<sub>2</sub>
  - Ships, liquefied CO<sub>2</sub>
  - Barges



# Physical properties of liquid CO<sub>2</sub>

- Low viscosity liquid, almost like water, density about 1.1 t/m<sup>3</sup>
- Liquid only under pressure
- Triple point @ -56,6 °C and 4,17 barg (5,18 bara)
- Dry ice, density 1,6 t/m<sup>3</sup> and -80 °C
- Critical point @ 31 °C and 73 barg
- Not miscible with water, but somewhat soluble





# CO<sub>2</sub> in dense phase

- Dense phase = supercritical CO<sub>2</sub> at pressures near or above 73 baro and near or under 31 °C
- Supercritical CO<sub>2</sub> has no definite or visible transitions between liquid, dense and gas
- Dense phase CO<sub>2</sub> has a density of  $900 \pm 100 \text{ kg/m}^3$  and behaves as a compressible liquid



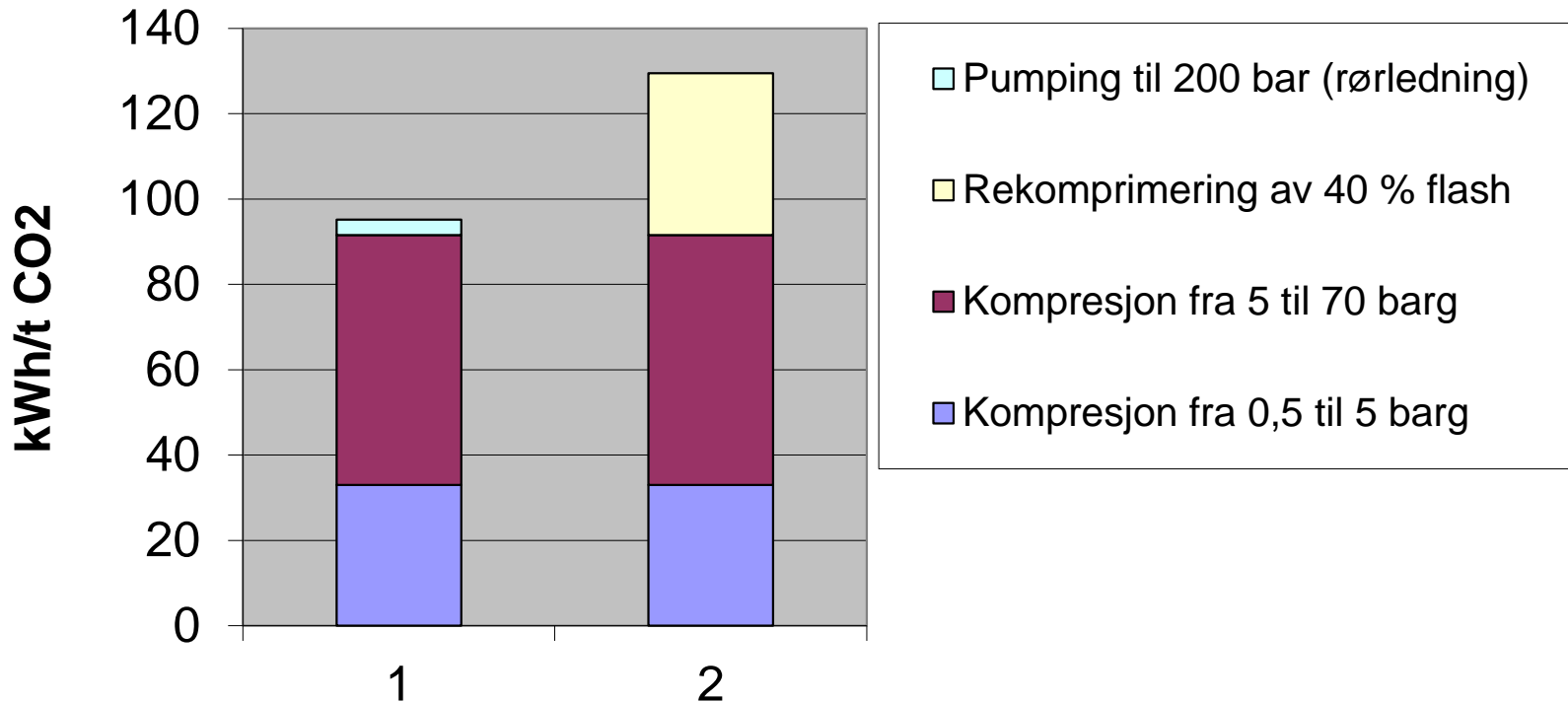
# Transport conditions

- Dense phase CO<sub>2</sub> in pipeline:
  - >80 barg, 25 °C, <600 ppmv H<sub>2</sub>O
- Compressed CO<sub>2</sub> on ship:
  - 40 - 80 barg, 0 - 25 °C, <600 ppmv H<sub>2</sub>O
- Liquefied CO<sub>2</sub> on ship:
  - 5,8 barg, –50 °C <50 ppmv H<sub>2</sub>O

# Preparation for transport: Energy need

1. Compressed CO<sub>2</sub> for transport in pipeline or ship

2. Liquefied CO<sub>2</sub> at -50 °C





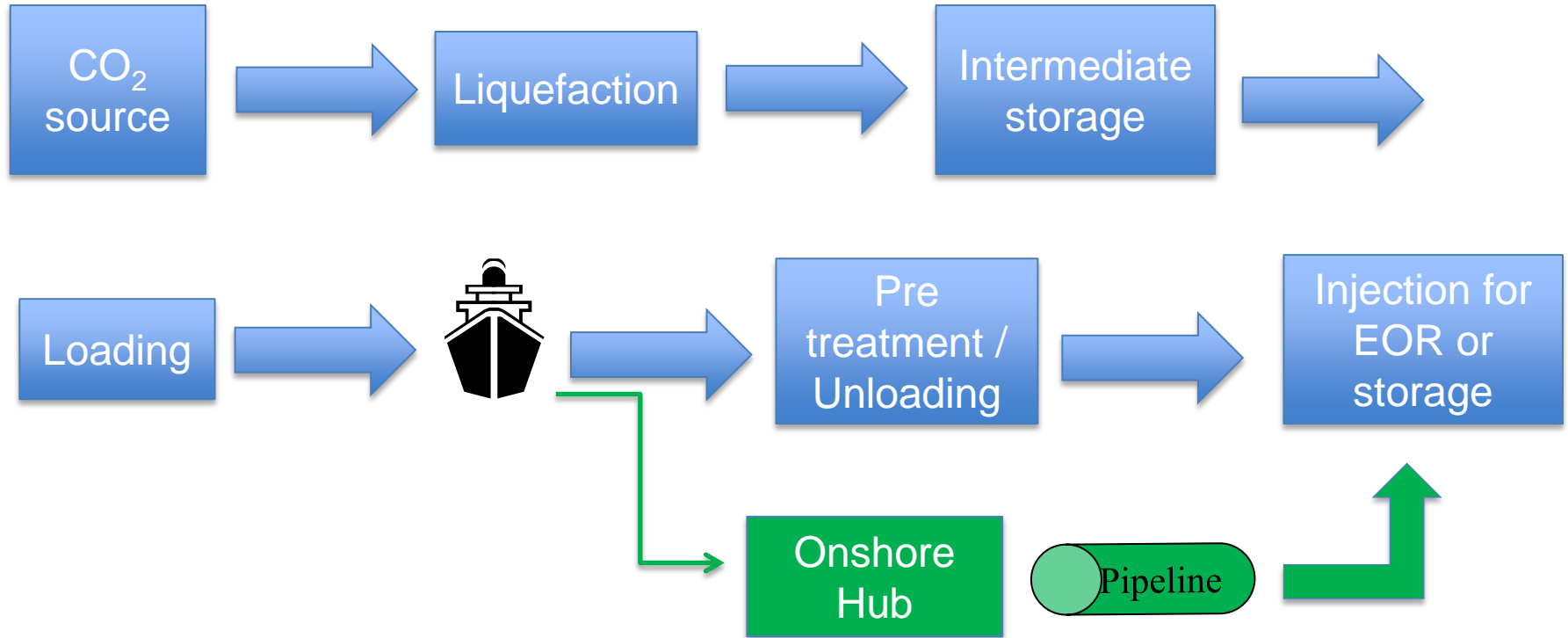
# Ship size and installations on land

- Optimal size of ship vary with transporting distance and CO<sub>2</sub> volume
  - 10000 – 50000 tons of cargo?
- CO<sub>2</sub> to be liquified (7 barg, -50°C, <50 ppm H<sub>2</sub>O)
- Need of intermediate storage tanks, capacity about +50% of ship
- Need of loading facilities





# Ship based CCS chain



# Existing CO<sub>2</sub> ship

Food grade CO<sub>2</sub> transport

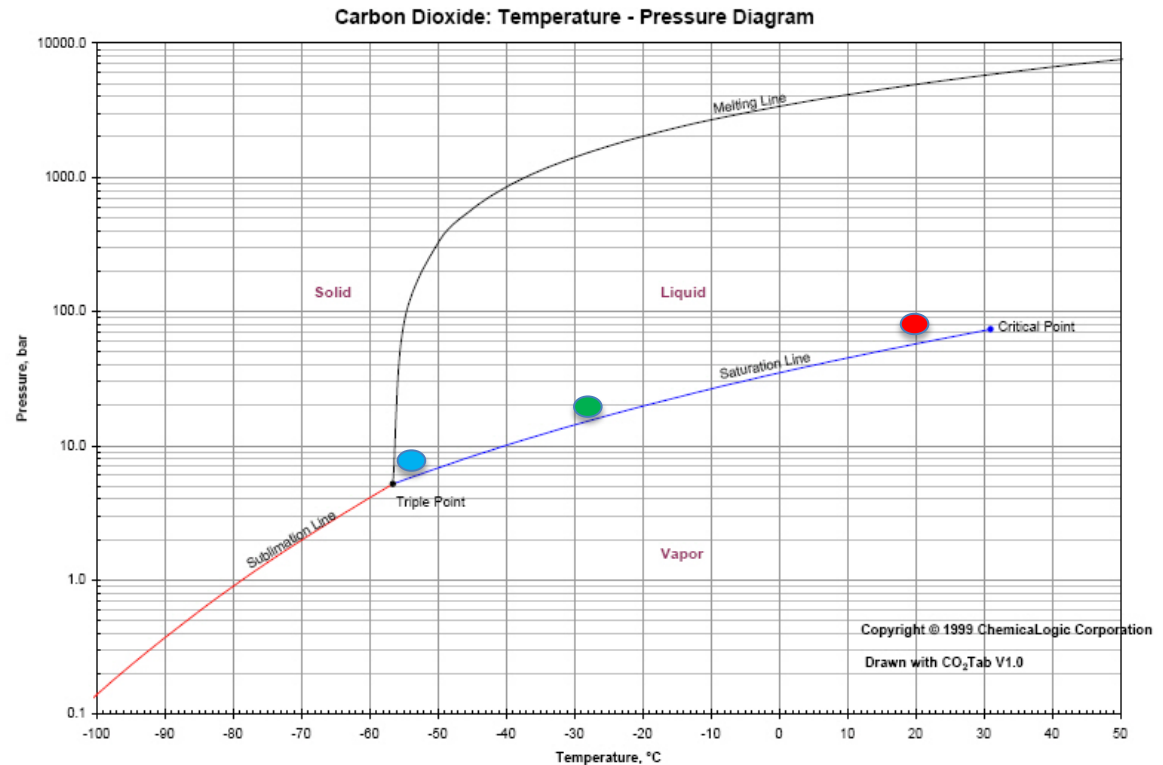


M/T Yara Gas III alongside the quay near Yara's ammonia plant in Porsgrunn,  
Capacity: 1200 t of liquefied CO<sub>2</sub> in 2 tanks of 600 tons capacity each  
Ship type: Converted container vessel

# Ship transport of CO<sub>2</sub> (1)

- Ships or barges carrying
  - liquefied CO<sub>2</sub>
  - compressed CO<sub>2</sub>

- Liquefied
- Compressed
- Commercial





## Ship transport of CO<sub>2</sub> (2)

- Commercial maritime transport of CO<sub>2</sub>
  - Ongoing for years
  - Small quantities
  - CO<sub>2</sub> is used for food and beverages, cleaning, fire extinguishers etc.
  - Transport conditions are;  
15 – 18 bar, -22 to -28°C (liquefied)



# Offshore unloading to buoy, platform



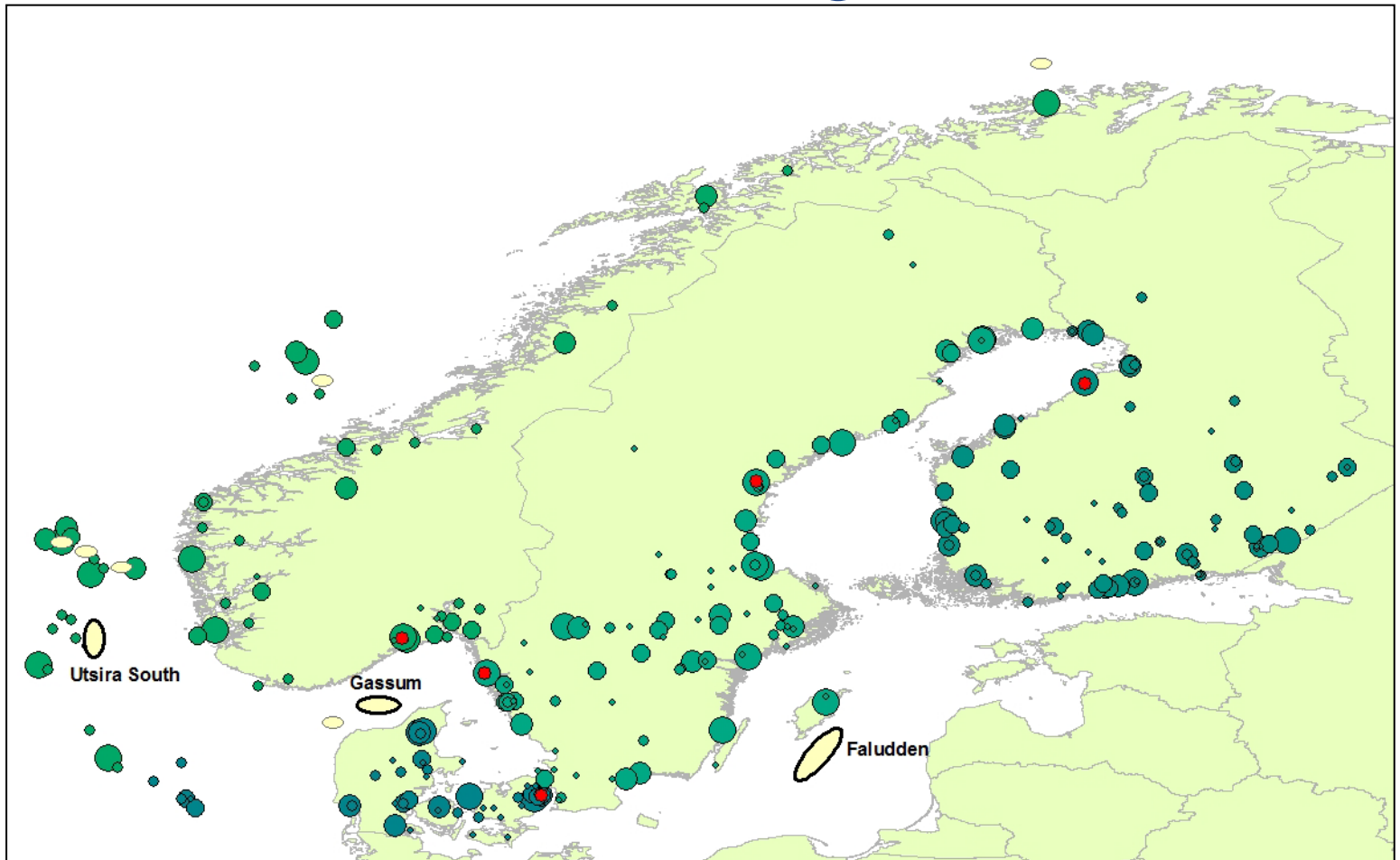


# EOR vs. aquifer storage

- EOR
  - Limited injection period
  - CO<sub>2</sub> injection rate is gradually reduced
    - Produced CO<sub>2</sub> is re-injected
    - Offset options must likely be in place
  - Needs reliable supply of CO<sub>2</sub>
  - Considered to be a stepping stone for implementation of CO<sub>2</sub> storage in saline aquifers



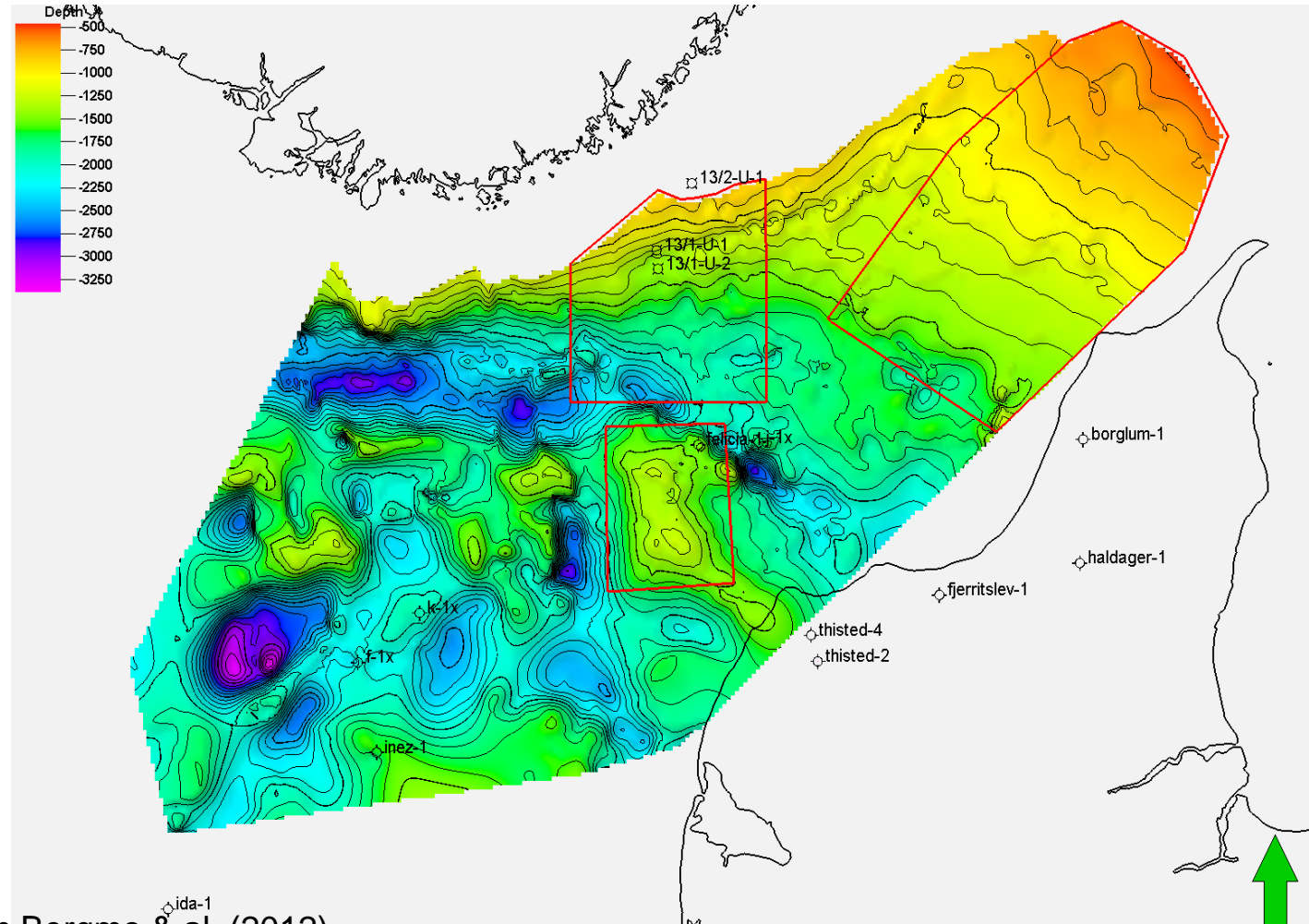
# CO<sub>2</sub> sources and possible storage sites in the Nordic region



Green: Fossil sources, Red: biogenic sources,  
Yellow: Possible storage sites



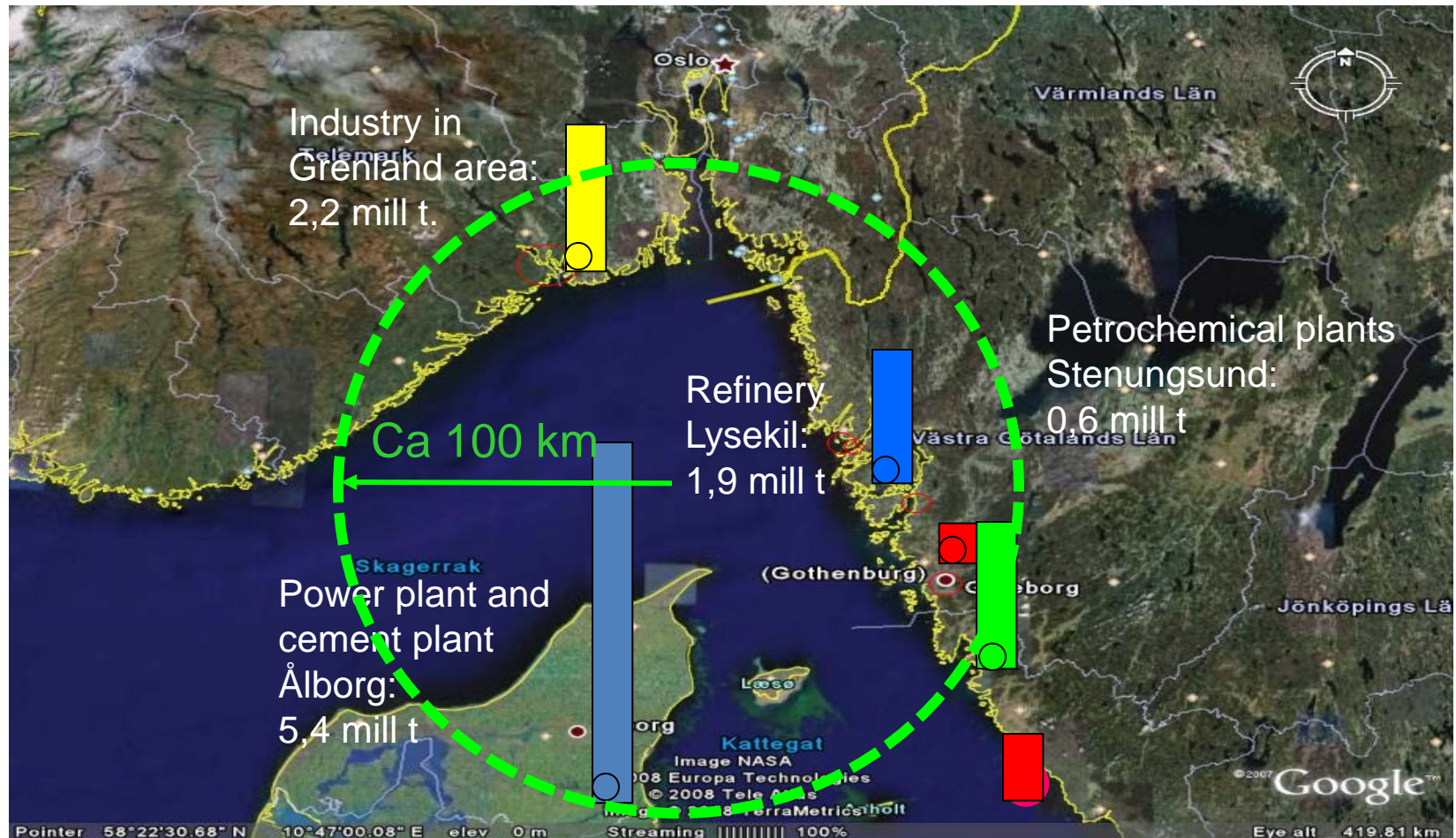
# Depth contour map of top Gassum formation and examined storage models



From Bergmo & al. (2012)

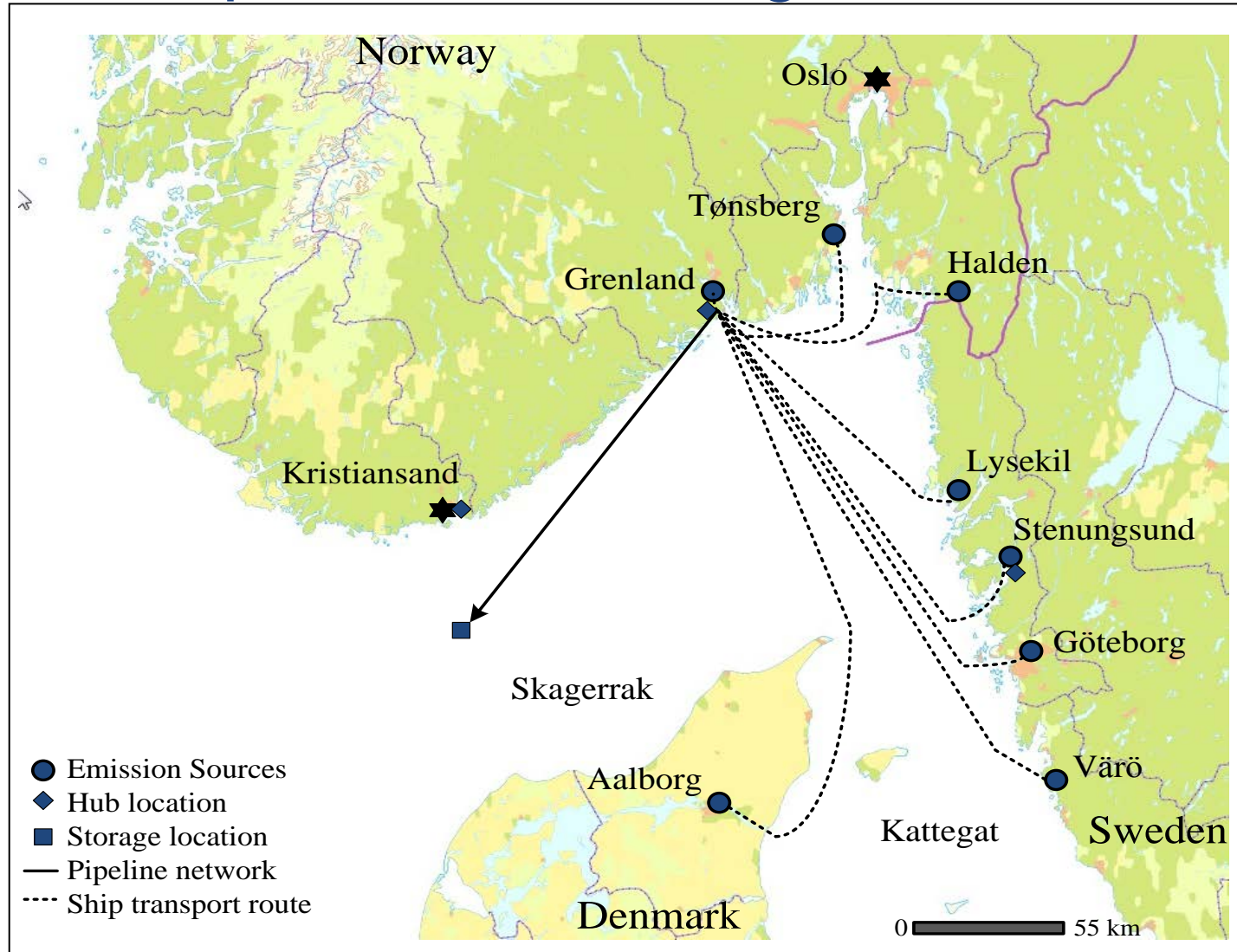
# Large CO<sub>2</sub> point sources in the Skagerrak / Kattegat region

Total emissions from large point sources: Approx 13 mill tonnes CO<sub>2</sub>/year



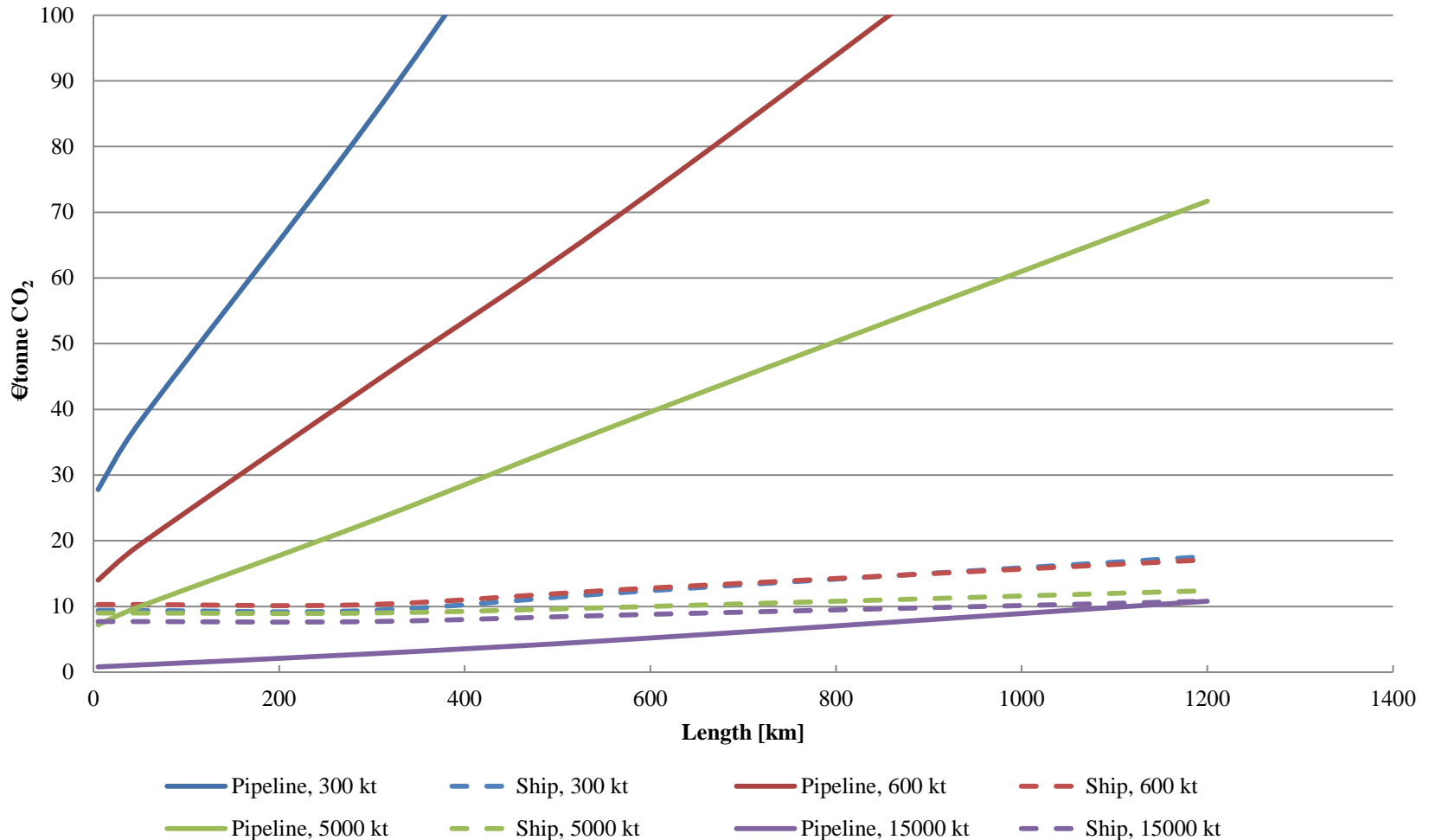


# Combination of ships and pipelines: An example from the Skagerrak area



# Transport cost generic comparison

## Cost variation with length and capacity





# Transport cost – ramp up

- Unless building strict one-to-one pipelines, 100% capacity utilization from day 1 is very unlikely
- Alternative solutions:
  - Replace pipelines concurrently with increasing CO<sub>2</sub> volumes
  - Parallell pipelines
  - One oversized pipeline from day 1
    - Challenges:
      - Reasonable knowledge of future CO<sub>2</sub>-volumes
      - Who to pay for redundant capacity until full volume?
  - Ships





# Cost impact of the main elements of the CCS chain

Part of CCS chain	Eur/tonne	Significant cost parameter
Capture	50-60	Energy cost
Transport-ship/pipeline	12	Liquefaction plant, storage and volume
Transport-pipeline	14	Volume, utility
Storage	9	Number of injection wells



# CO<sub>2</sub>-transportation, ships vs. pipelines

<i>Pipelines</i>		<i>Ships</i>	
<i>+</i>	<i>-</i>	<i>+</i>	<i>-</i>
<i>Low Opex</i>	<i>High Capex</i>	<i>Low Capex</i>	<i>High Opex</i>
<i>Onshore needs: Compression</i>	<i>Relatively low flexibility</i>	<i>Large flexibility (volume and route)</i>	<i>Onshore need for intermediate storage and liquefaction plants</i>
<i>Can be built both onshore and offshore</i>	<i>Low potential for re-use</i>	<i>Re-use potential</i>	
	<i>Large sunk cost</i>	<i>Lower sunk cost</i>	
		<i>Short delivery time (2 years ?)</i>	



# Why are ships crucial in establishing a CO<sub>2</sub> infrastructure?

- Flexible source-to-storage solutions
  - Including combination with pipelines
- Economy
  - Avoiding large up-front capex
  - Can also be combined with CO<sub>2</sub>-EOR
  - Smooth transition towards larger pipeline infrastructure
  - Ships may be re-built and re-used
- Faster road to implementation of CCS

Probably not a future CO<sub>2</sub> tanker

Thank you for your attention

